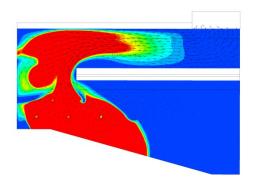


Moving Grate Combustion Optimisation with CFD and PIV (Particle Image Velocimetry)

Thomas Nussbaumer Martin Kiener

Bioenergy Research Group Lucerne University of Applied Sciences

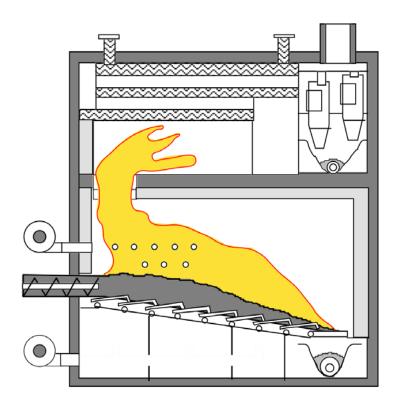




- 1. Introduction
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 - 3. Optimisation with CFD
 - 4. Comparison with PIV
 - 5. Experiments on a 1.2 MW boiler
 - 6. Conclusions



Moving grate boiler for biomass





Graph: Schmid energy solutions

Boiler capacity Fuel moisture Ash content Verenum 500 kW – 50 MW

10% - 60% (of wet mass)

0% - >10%

Limitations in practical operation

Load range for continuous operation from 40% – 100%

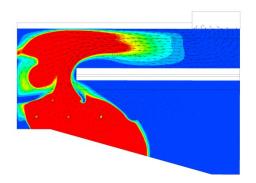
Consequence 1: Intermittent on/off operation at lower load

- Start phases cause increased emissions
- ESP or fabric filters may be off or in bypass

Consequence 2: Increase of CO and VOC at part load

 Interest to identify the reason(s): Mixing, temperature, uneven fuel distribution, others?

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The target is...

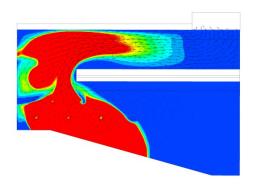
... to optimise the combustion

to ascertain low excess air and high efficiency and

... to improve the part load capability with increasing the load range to < 30% - 100%

... by aerodynamic optimisation, i.e.,1. secondary air injection and2. optionally with flow obstacles.





- 1. Introduction
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Method

- Solid Biomass conversion to gases (CO, CO₂, H₂, H₂O, CH₄) and char is calculated by a one-dimensional transient integral model in adaptation to [1] currently refined by [2]
- 2. Gas phase modelled with CFD by use of k- ε and EDM
- 3. Boundary conditions for the reference case:

Thermal firing capacity	1.4 MW
Boiler efficiency	85%
Fuel humidity	50%
Primary- and secondary air temperature	80°C
Excess air ratio	
Primary air λ_{PA}	0.72
Primary air λ _{ΡΑ} Secondary air 1 λ _{SΑ1}	0.86
Secondary air 2 λ_{SA2}	0.22
Total: $\lambda_{tot} = \lambda_{PA} + \lambda_{SA1} + \lambda_{SA2}$	1.80

[1] T. Klasen, K. Görner, 2nd int. Symp. On Inc. And Flue Gas Treatm., Sheffield 4.-6.7.1999
 [2] J. Martinez, T. Nussbaumer, Poster 2 DV 3.61

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Fluid dynamic parameters

Requirement 1: Turbulence Re =
$$\frac{u \cdot L}{v}$$
 > 2300

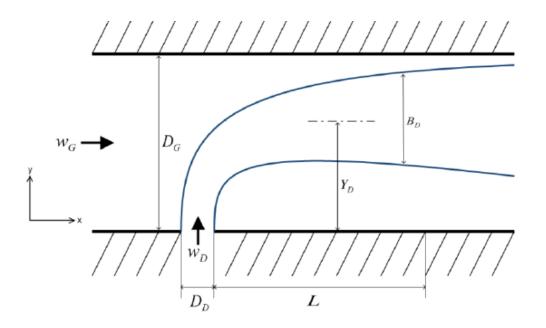
a) Design for turbulent flow (here ascertained as Re>>2300

b) For PIV:
$$Re_{Model} = Re_{Reality}$$



Fluid dynamic parameters

Requirement 2: For Mixing two fluid flows: Jet In Cross Flow, JICF [1,2]



[1] Schlüter, J.U.; Schönfeld, T.: *Flow, Turbulence and Combustion*, 65: 177-203; 2000[2] Suman, M, Thesis, University of Minnesota, USA; 2006]



Fluid dynamic parameters

Requirement 2: For Mixing two fluid flows: Jet In Cross Flow, JICF [1,2]

Impulse Ratio between flows = ratio of imp. current densities

a) Design for optimum IR
b) For PIV: IR_{Model} = IR_{Reality}

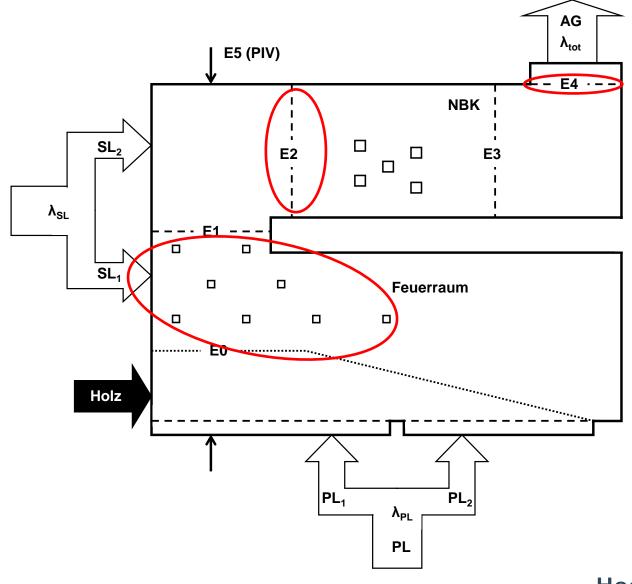
$$IR_{JM} = \sqrt{\frac{\rho_{J} \cdot u_{J}^{2}}{\rho_{M} \cdot u_{M}^{2}}}$$

 $\begin{array}{ll} u_J & \text{velocity of jet flow [m/s]} \\ u_M & \text{velocity of main flow [m/s]} \\ \rho_J & \text{density of jet flow [kg/m^3]} \\ \rho_M & \text{density of main flow [kg/m^3]} \end{array}$

[1] Schlüter, J.U.; Schönfeld, T.: *Flow, Turbulence and Combustion*, 65: 177-203; 2000[2] Suman, M, Thesis, University of Minnesota, USA; 2006]



CFD Analysis





Results CFD: 1. Full load / part load

CO (part load) < CO (nominal load)

Explanation: – Impulse ratio remains constant – Turbulence is ensured also at part load

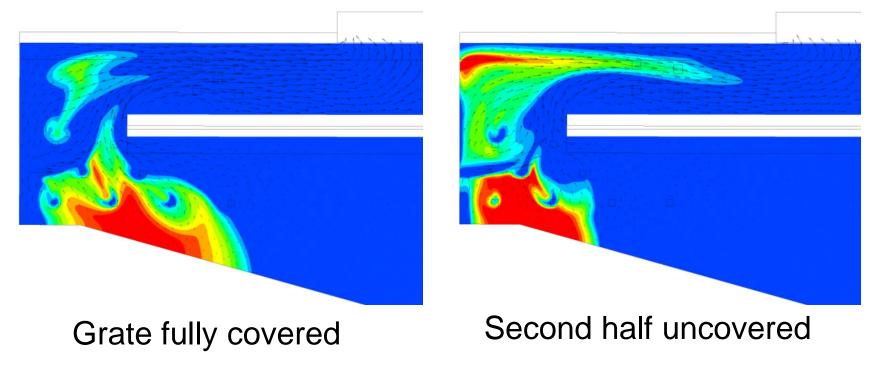
However, only at identical boundary conditions, i.e.,

- temperature,
- excess air ratio, and
- grate coverage



Results CFD: 2. Grate coverage

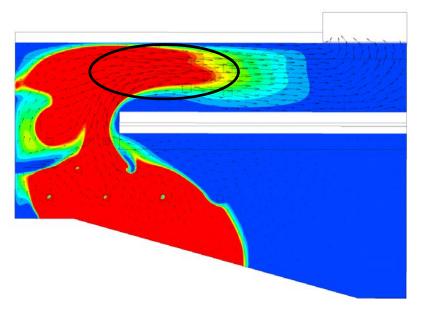
Reference case

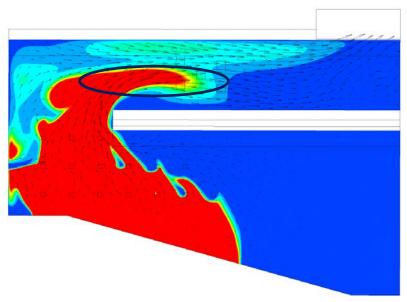




Results CFD: 3. Secondary air injection

Reference case





Case SL-8

N = 1 A = 1 $\Delta p = 100\%$ $CO_{P4} = 100\%$ N = 2 A = 1 $\Delta p = 97\%$ $CO_{P4} = 42\%$



Selection of cases for experiments 1. Secondary air injection

Case	EXP	N/N _{ref} [-]	A _N /A _{N,ref} [-]	A _{tot} /A _{tot,ref} [-]	ir _{norm} [-]	CO/CO _{ref} [%]	ME/ME _{ref} [%]	∆p/∆p _{ref} [%]
SA-1			1	0.125	8	0.1	99	6630
SA-2			0.25	0.25	4	2	100	1647
SA-3	+	1	0.5	0.5	2	21	101	405
Ref	+		1	1	1	100	100	100
SA-4			2	2	0.5	252	96	23
SA-5			0.0625	0.125	8	0.1	92	6464
SA-6			0.125	0.25	4	0.1	100	1683
SA-7		2	0.25	0.5	2	3	98	405
SA-8	+		0.5	1	1	42	97	97
SA-9			1	2	0.5	199	95	23
SA-10	+	1.5	0.5	0.75	1.33	—	-	-

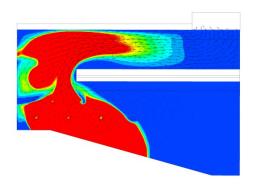
*ME = Mixing Efficiency: The local mixing quality of two flows is defined as difference between the local tracer concentration and the mean tracer concentration of a fully mixed flow [Baillifard, M. et al.: 16th EU Conf., Valencia, 2–6 June 2008]

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Selection of cases for experiments 2. Obstacles

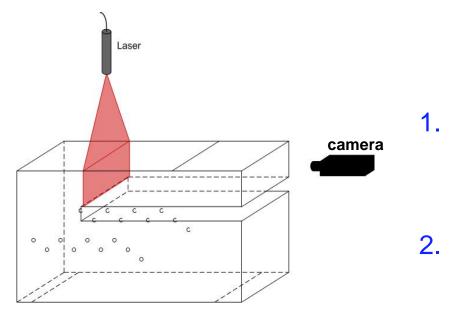
Case	EXP	Variation	CO/CO _{ref} [%]	ME/ME _{ref} [%]	∆p/∆p _{ref} [%]
Ref	+	No	100	100	100
O-1		Narrow deflection	26	105	138
O-2	+	Obstacle middle	27	103	132
O-3		Obstacle after SA ₂	106	99	103
O-4	+	Obstacle side	20	106	141
O-5		Asym. obstacle in PCC	57	103	137
O-6		Neck in P1	38	104	113
O-7		Nose before deflection	126	98	97
O-8	+	Obstacle ceiling	11	104	222





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- Flow seeding by tracer aerosols (1 μm)
 for flow field detection in general
 in one flow of two for mixing process
- 2. Illumination of plane with laser



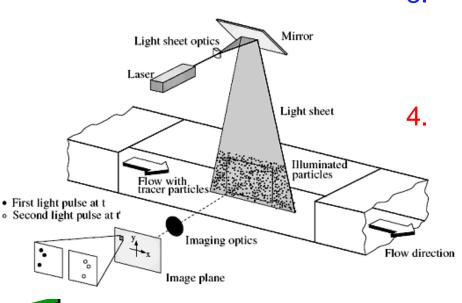
- Flow visualisation by tracer aerosols

 for flow field detection in general
 - in one flow of two for mixing process
- 2. Illumination of plane with laser
- 3. Image recording with 1 camera for 2D flow field

with 2 cameras for 3D flow field

- Two pictures in a series of 20 μ s to 2 ms to identify
 - velocity and
 - direction of each tracer
 by statistical data analysis

Hochschule Luzern Technik & Architektur

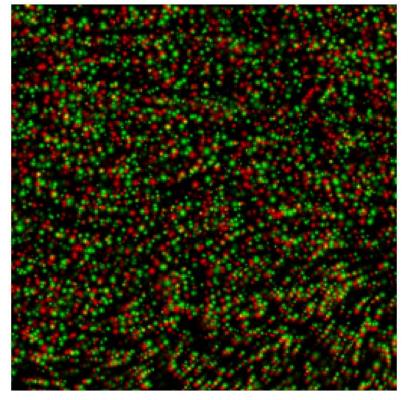


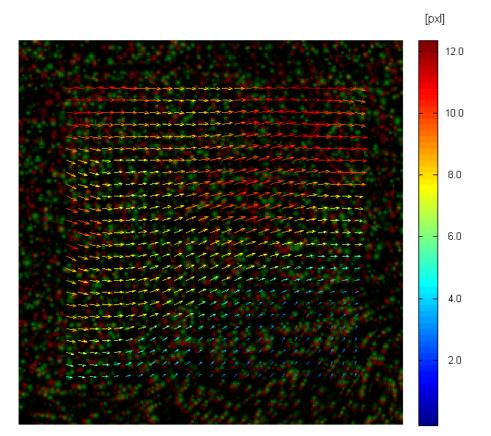
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Superposition of two images

Vector map

red: image 1 green: image 2



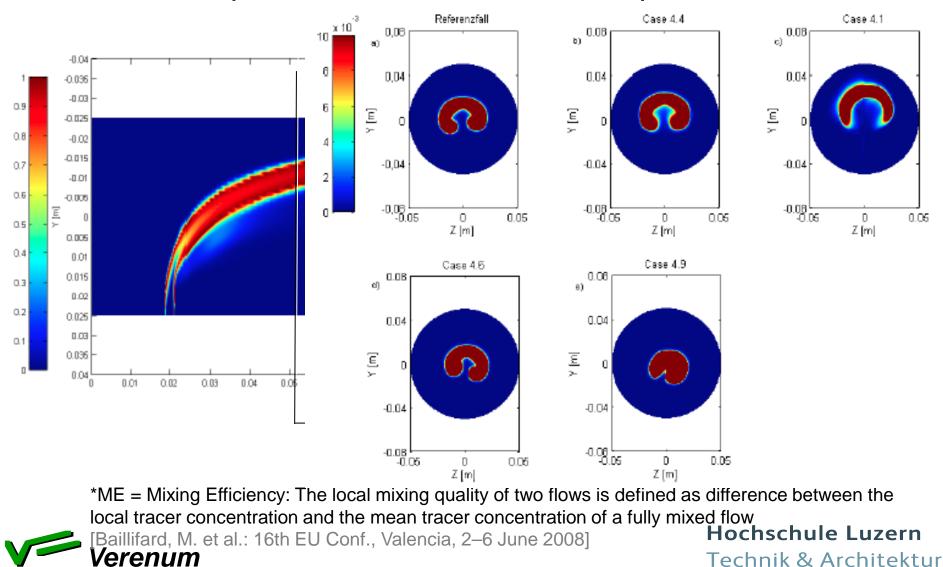




[Institute for Fluid Dynamics IFD at ETH Zurich]

Particle Image Velocimetry (PIV) - Example

Mixing Efficiency of Jet In Cross Flow, JICF Penetration dephts and area for different impuls ratios IR



Reality



Scaled model for PIV

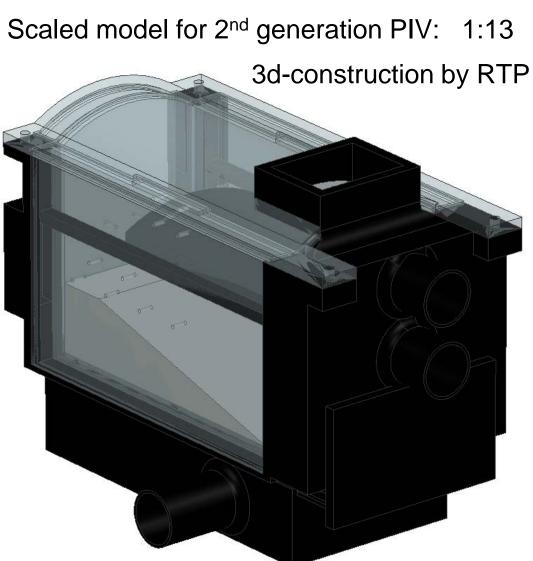
- 1. Geometrical similarity
- 2. Kinematical similarity
- 2. Dynamical similarity

Similarity analysis of dimensionless numbers:

	Reality	Model	Effect
Reynolds Re	26 500	26 700	Turbulence, flow conditions
Schmidt Sc	0.77	0.76	Diffusion
Mach Ma	0.02	0.16	Incompressible fluid < 0.3
Impulse ratio IR x D _{norm}	0.30	0.29	Penetration depth of jet in cross flow (JICF)

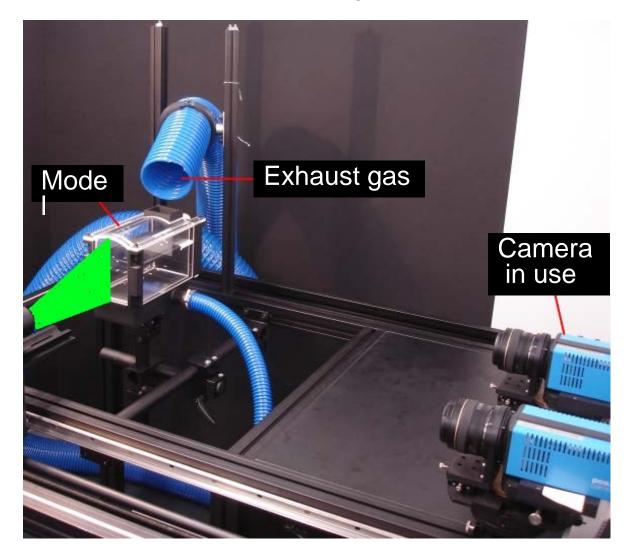






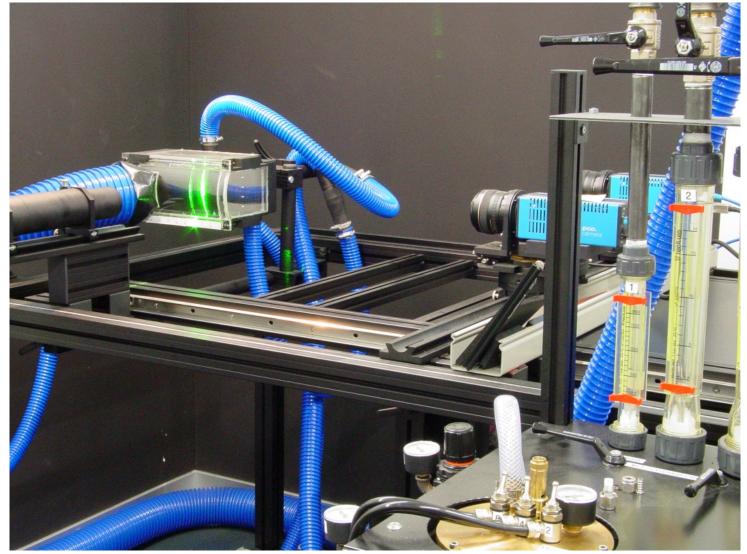


Scaled model for 2nd generation PIV: 1:13



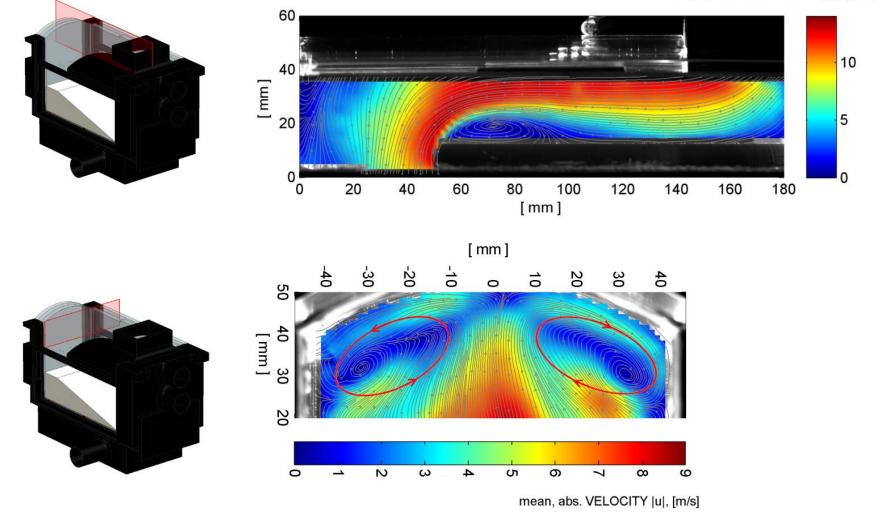


Scaled model for 2nd generation PIV: 1:13

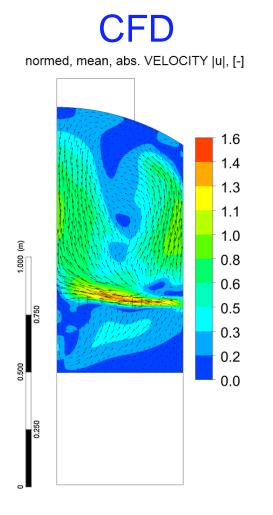


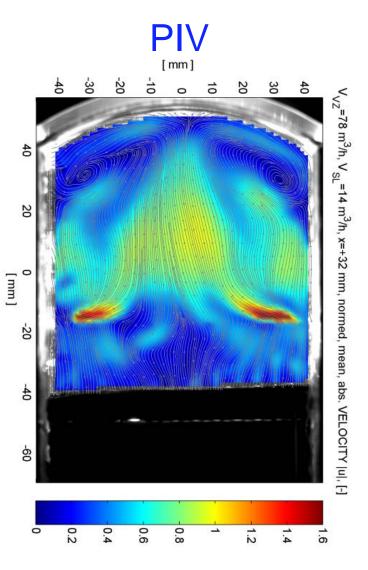


mean, abs. VELOCITY |u|, [m/s]

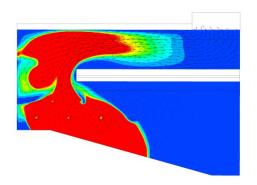












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1.2 MW Moving grate boiler



Operation with ideal grate coverage (80%)

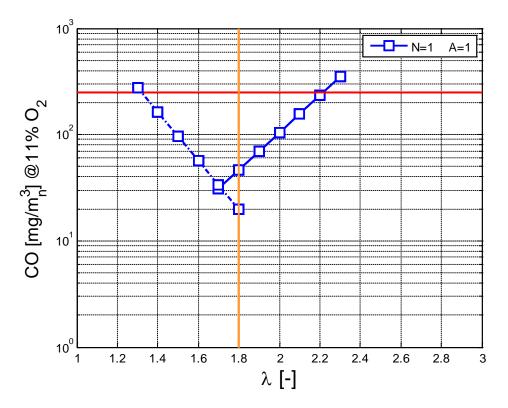


Load ≈ 20%



1. Influence of secondary air injection

Full load

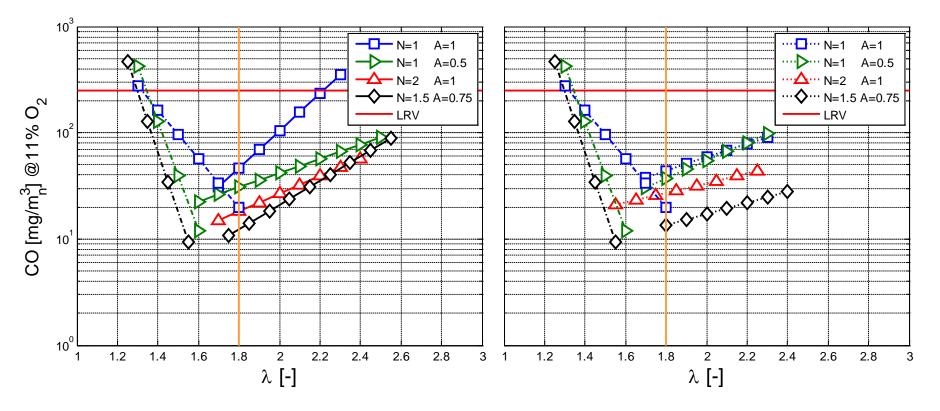




1. Influence of secondary air injection

Full load

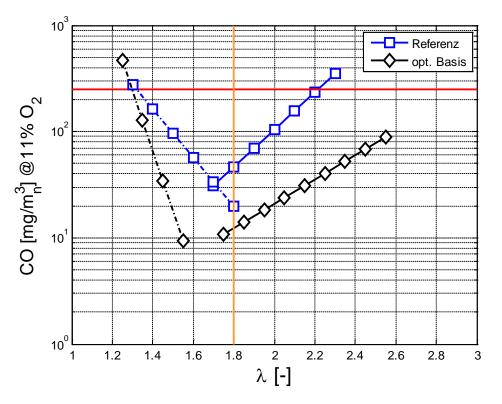
Part load



V Verenum

2. Influence of obstacles

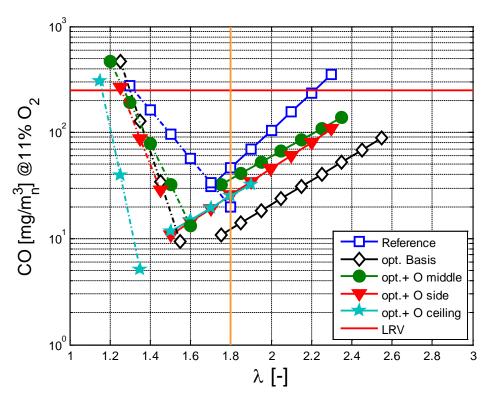
Full load





2. Influence of obstacles

Full load



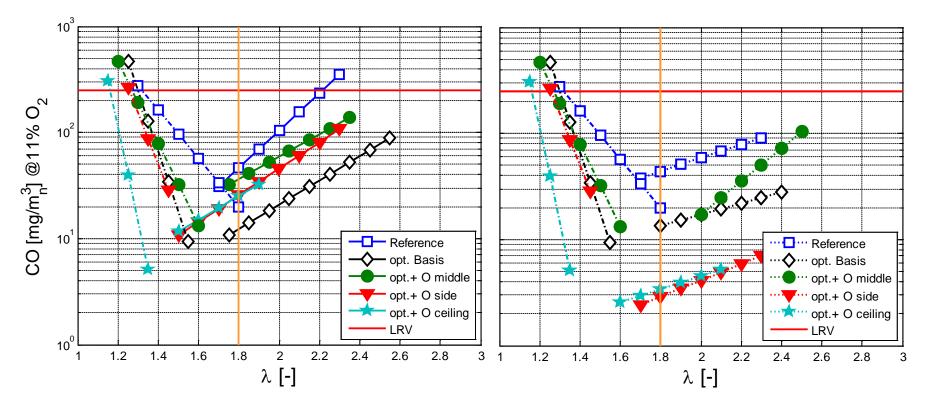




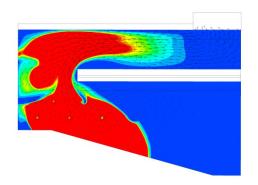
2. Influence of obstacles

Full load

Part load



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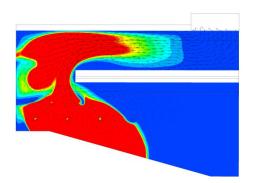


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- 1. The CO increase in part load on the investigated grate is not due to reduced turbulence but due to a an incomplete grate coverage. This can be reduced by grate and air control.
- 2. Optimised secondary air injection reduces CO both in full load and part load by around a factor of 4
- By exploiting the optimisation potential, stable operation from < 30% load to full load is achieved with CO < 15 mg/m_n³ (11% O₂)
- 4. Simultaneously the optimal excess air ratio is lowered from $\lambda = 1.7$ to $\lambda = 1.5$, which increases the efficiency
- 5. CFD is powerful to rapidly predict flow optimisation measures.
- 6. PIV is useful to validate CFD and also to test complex situations on scaled models, however, similarity needs to be considered.
- 7. The impulse ratio is confirmed to be a key parameter for mixing.





Acknowledgements

Swiss National Science Foundation SNSF

Commission for Technology and Innovation CTI

Schmid AG energy solutions



End of presentation

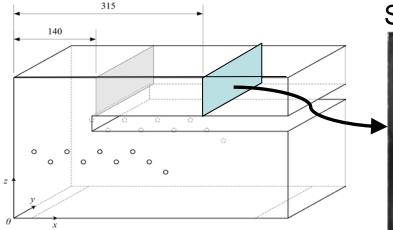
Scaled model for 1st generation PIV: 1:5 2d-construction



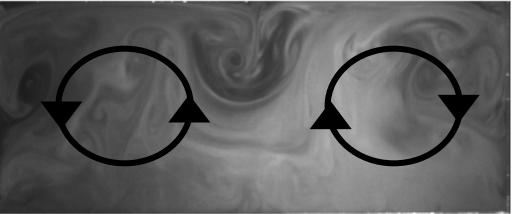


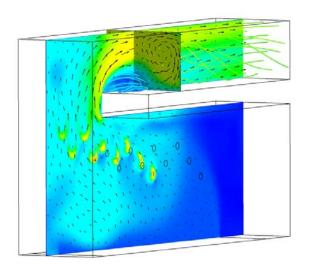
Institute for Fluid Dynamics IFD at ETH Zurich [Baillifard, M. et al.: 16th EU Conf., Valencia, 2–6 June 2008]

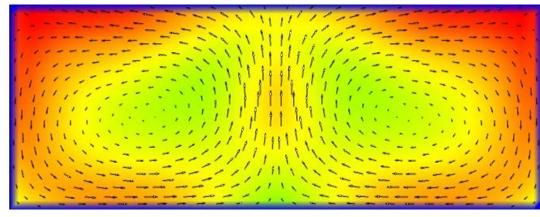




Scaled model for 1st generation PIV: 1:5

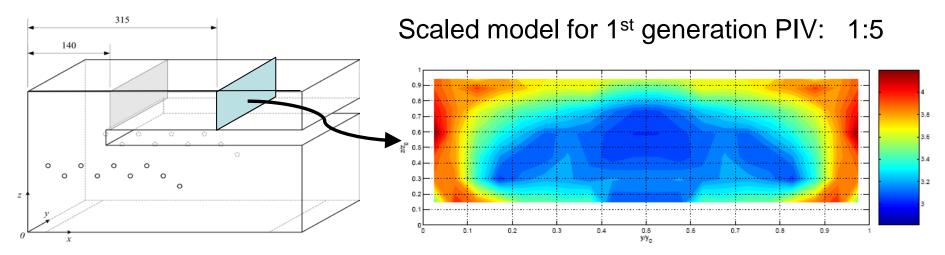


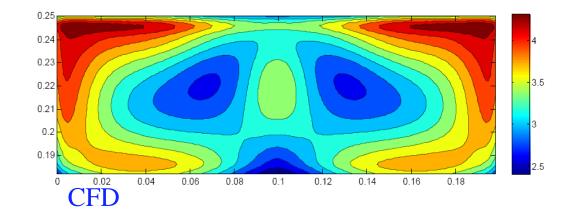




CFD







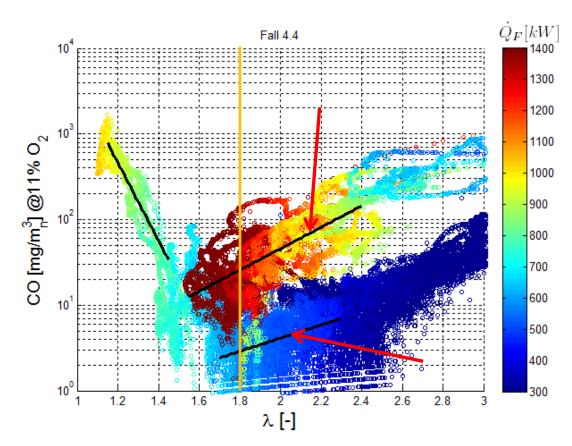
VerentarionM. et al.: 16th EU Conf., Valencia, 2–6 June 2008]

Interpretation

- Stationary phase with similar conditions:
 - PA/PA_{Ref}
 - PA/SA1
 - SA_1/SA_2
- Comparison of the cases in part and full load :

1. CO/Lambda-Diagram are approximated logarithmically

2. CO-value at $\lambda_{tot} = 1.8$ as reference value

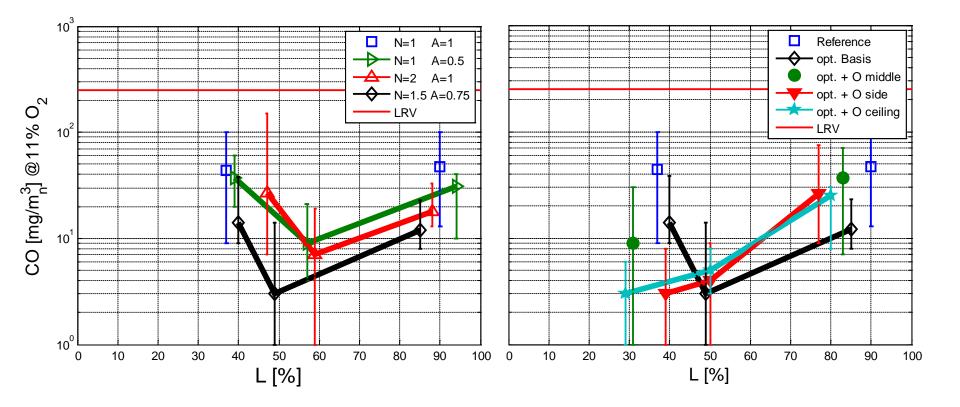




3. CO at λ =1.8 as function of the load

Without obstacles

With obstacles





Ideal grate coverage of 90% at 15% load





Non-ideal grate coverage at 40% load with uncovered sections at the end





Measurements

- Gas composition (O₂, CO₂, CO)
- Flue gas volume flow (Δp with pitot tube)
- Combustion air volume flows PA₁, PA₂, SA₁, SA₂ (heated wire anometry)
- Combustion temperature (PT100 in ceramic tube)
- Flue gas temperature (thermoelement)
- Excess air ratio
- Thermal firing capacity

