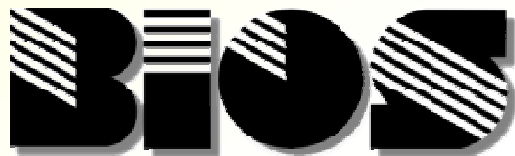


# Particle precipitation in medium- and large-scale biomass combustion plants

Thomas Brunner, Manfred Lixl



**BIOENERGIESYSTEME GmbH**

Infeldgasse 21b, A-8010 Graz, Austria

TEL.: +43 (316) 481300; FAX: +43 (316) 4813004

E-MAIL: [office@bios-bioenergy.at](mailto:office@bios-bioenergy.at);

HOME PAGE: <http://www.bios-bioenergy.at>





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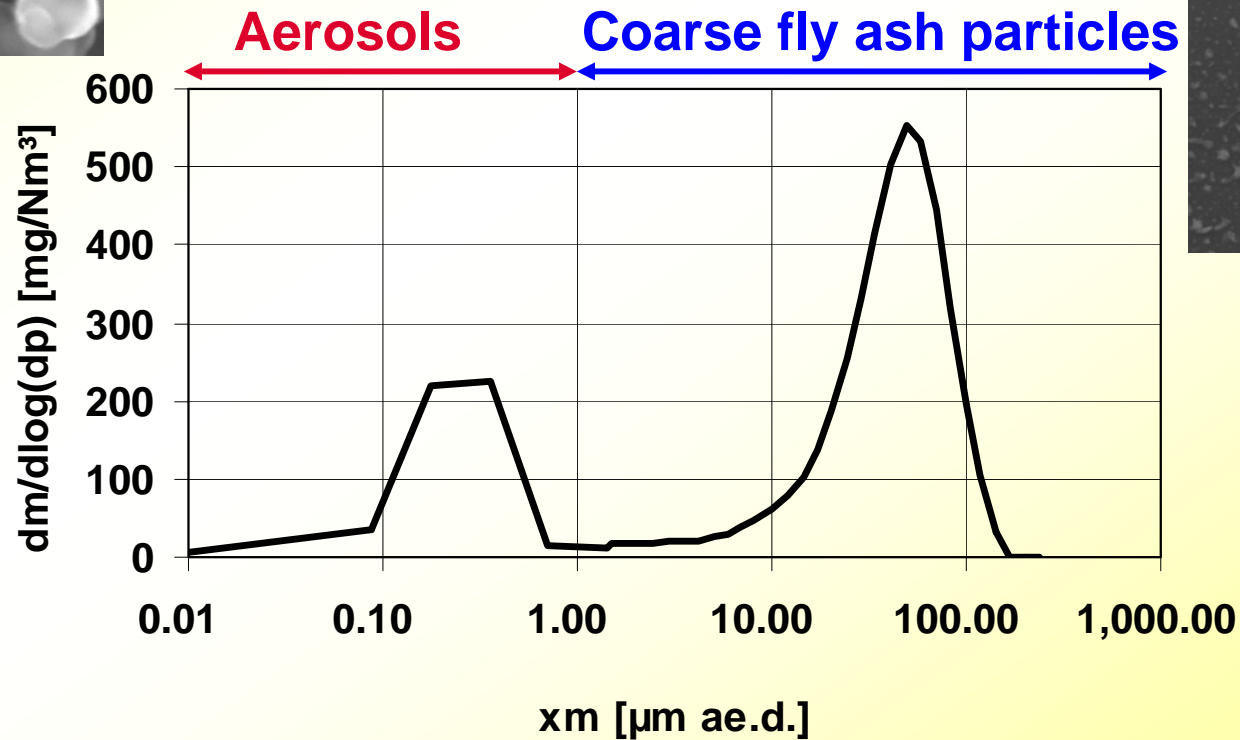
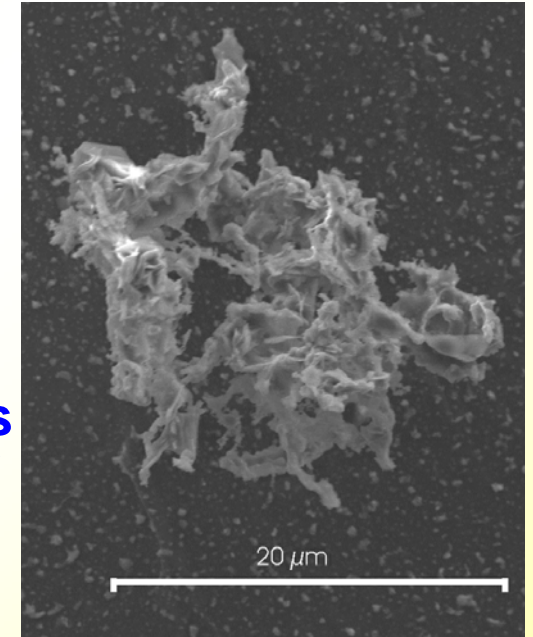
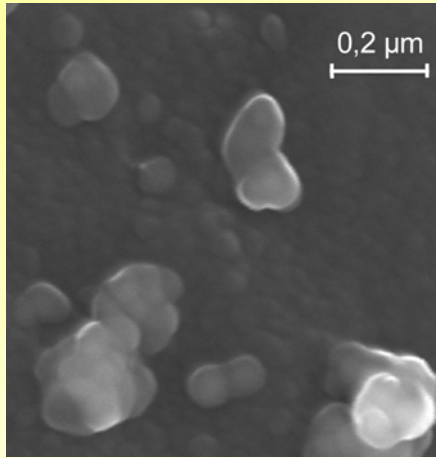
## Content

- **Characterisation of particles to be precipitated**
- **Technological description of different dust precipitation technologies**
- **Evaluation of the aerosol precipitation efficiencies of different dust precipitation technologies**
- **Recommendations concerning the application of different dust precipitation technologies in biomass combustion plants**



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# Typical particle size distributions of fly ashes formed during biomass combustion





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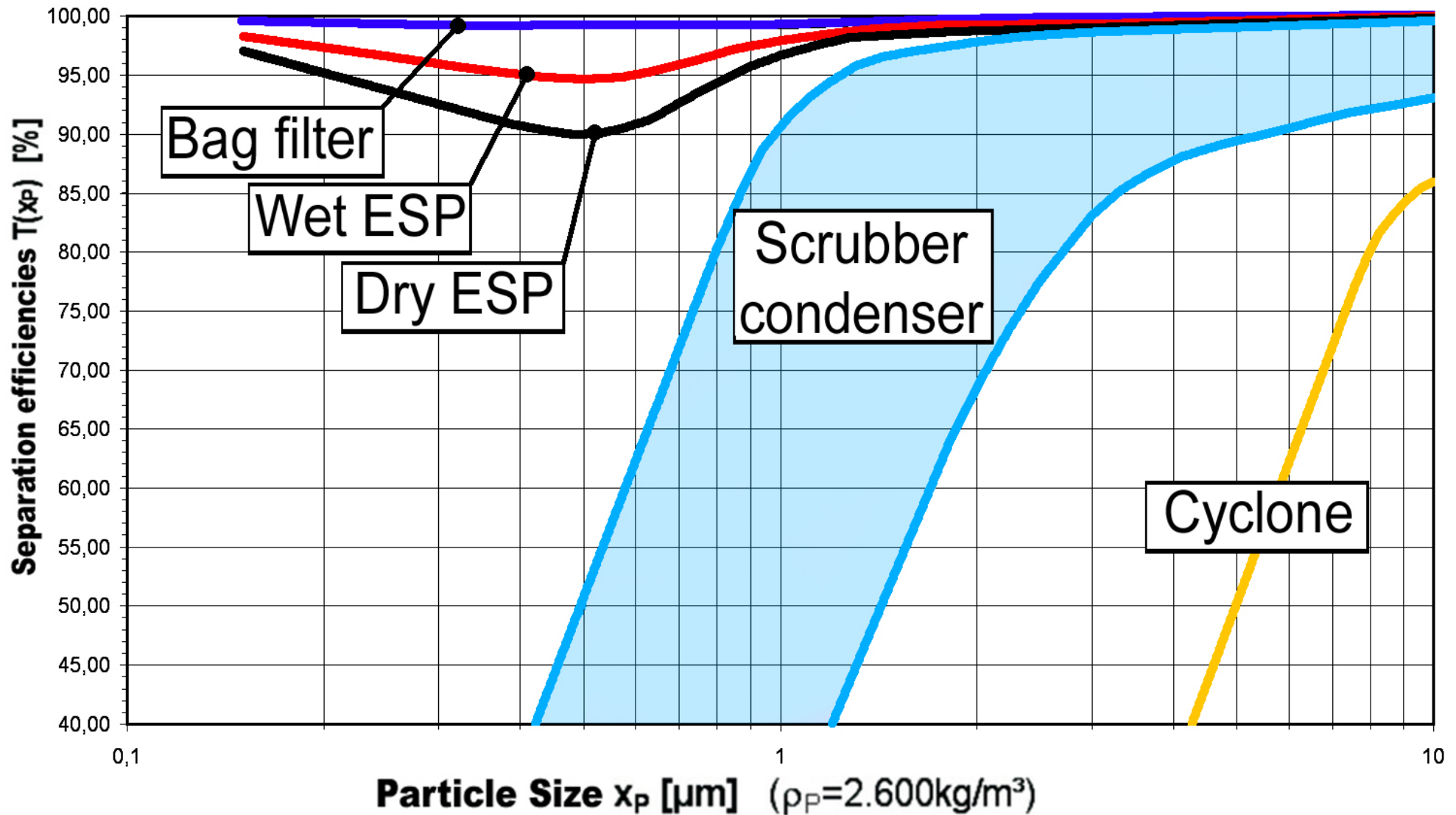
## Dust precipitation technologies – overview

- **Cyclones**
- **Multi-cyclones**
- **Flue gas condensation units**
- **Electrostatic precipitators (ESP)**
  - **dry ESP**
  - **wet ESP**
- **Baghouse filters**



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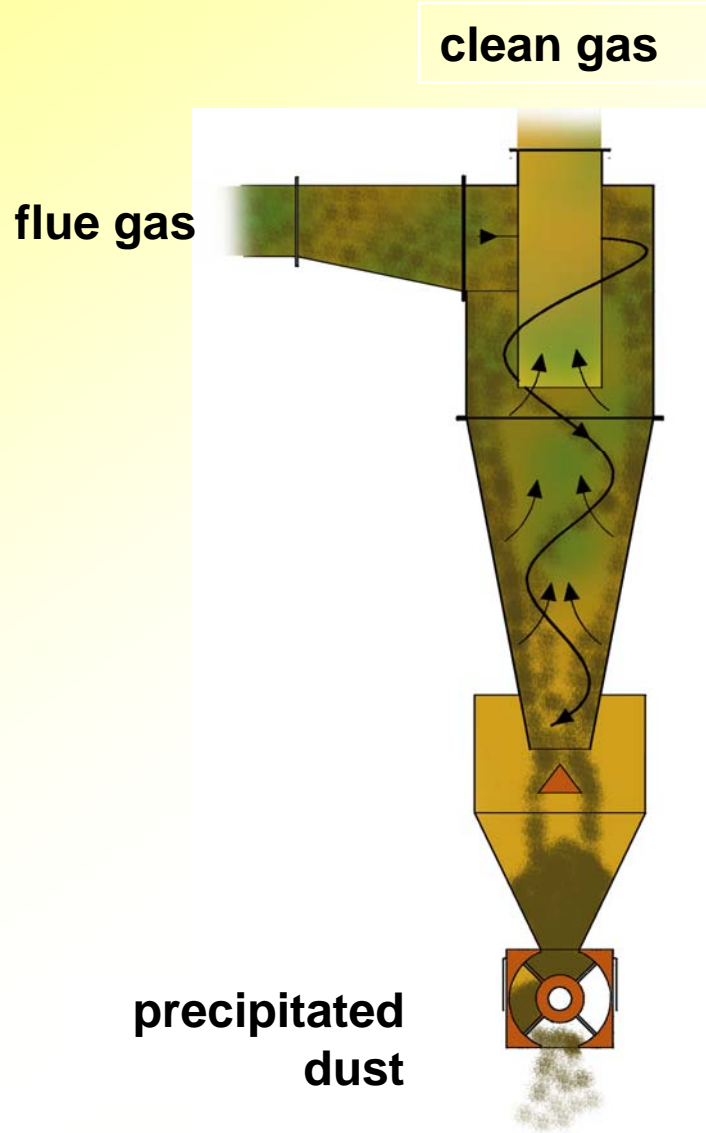
# Precipitation efficiencies of different dust precipitation technologies





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## Cyclones and multi-cyclones



### Principle:

precipitation by centrifugal forces

### Cut diameters:

~ 5  $\mu\text{m}$

### Operation temperature:

- up to 1,300 °C
- usually 150 - 250°C

### Operation pressure:

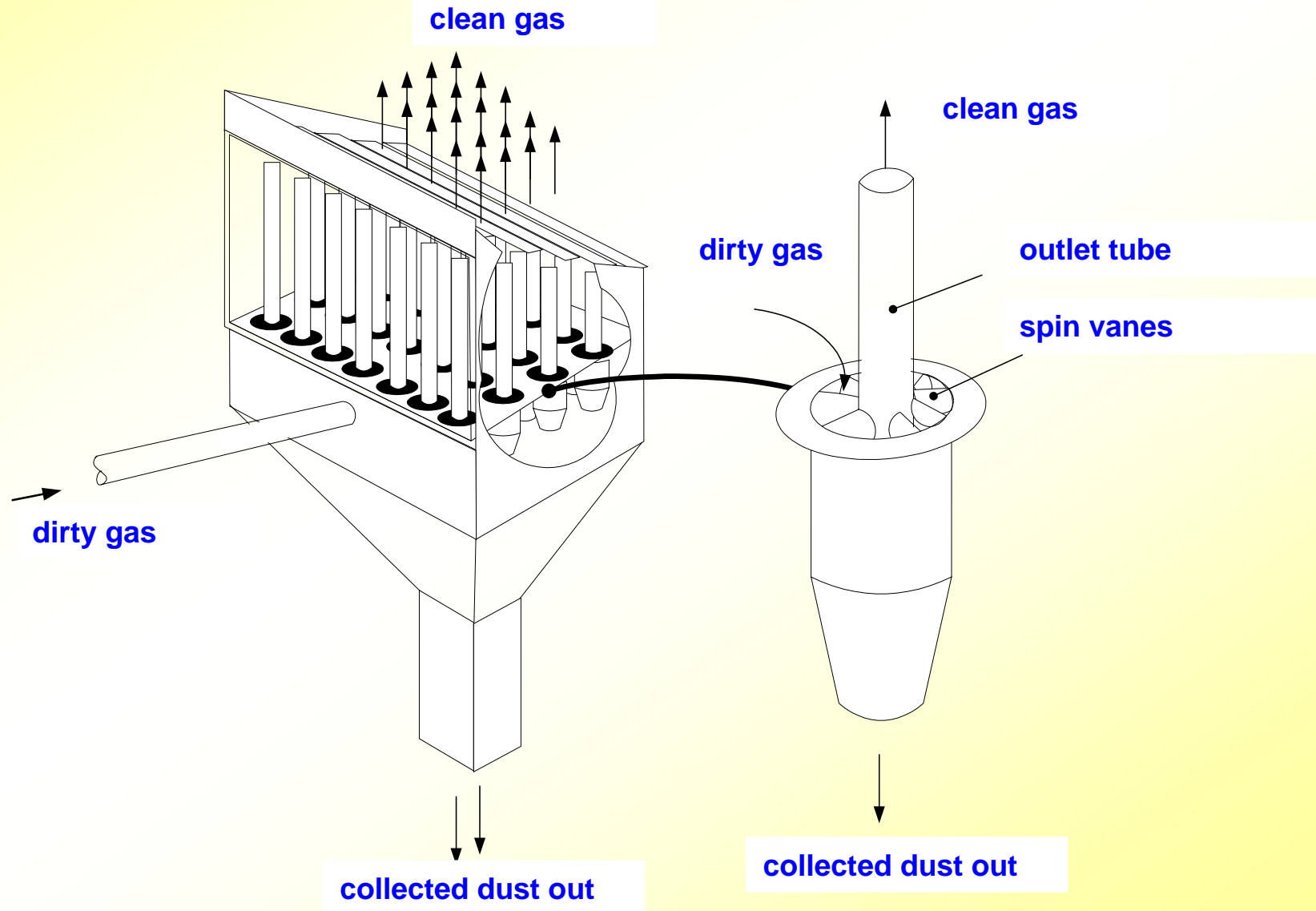
- up to 100 bar
- usually atmospheric

**Only suitable for coarse fly ash precipitation**



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## Scheme of a multi-cyclone

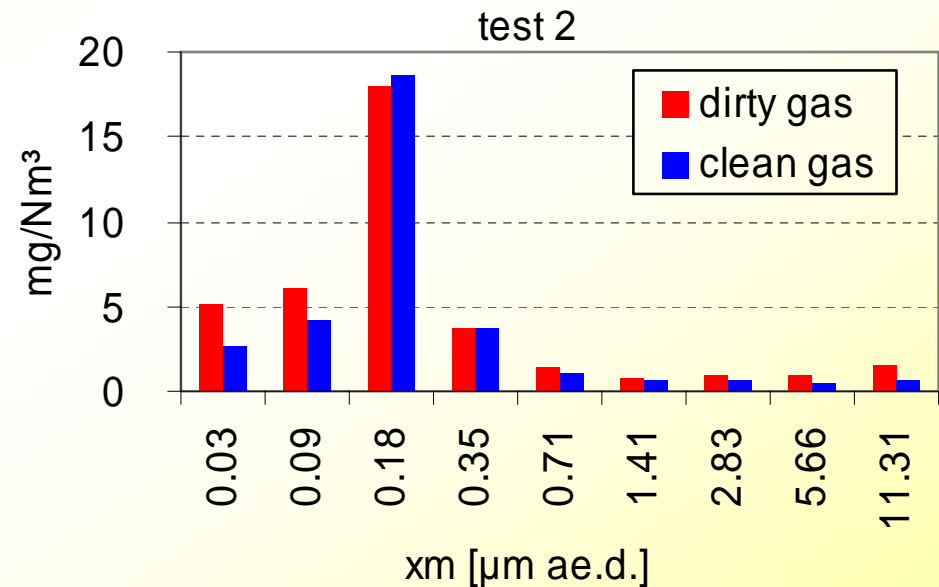
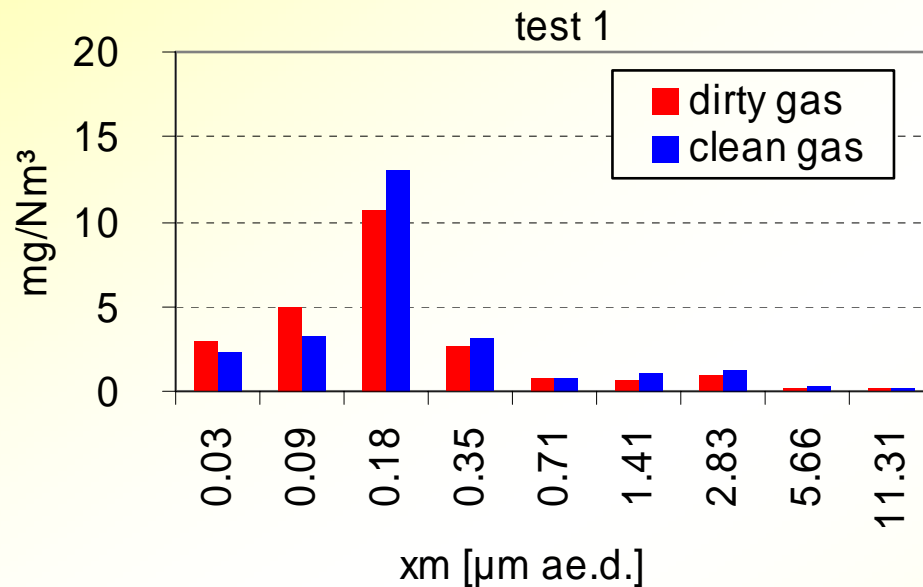




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## Multi-cyclones – aerosol separation

### Measured particle size distributions of aerosols upstream and downstream a multi-cyclone (coarse fly ashes are not considered)



### Almost no separation of aerosol particles

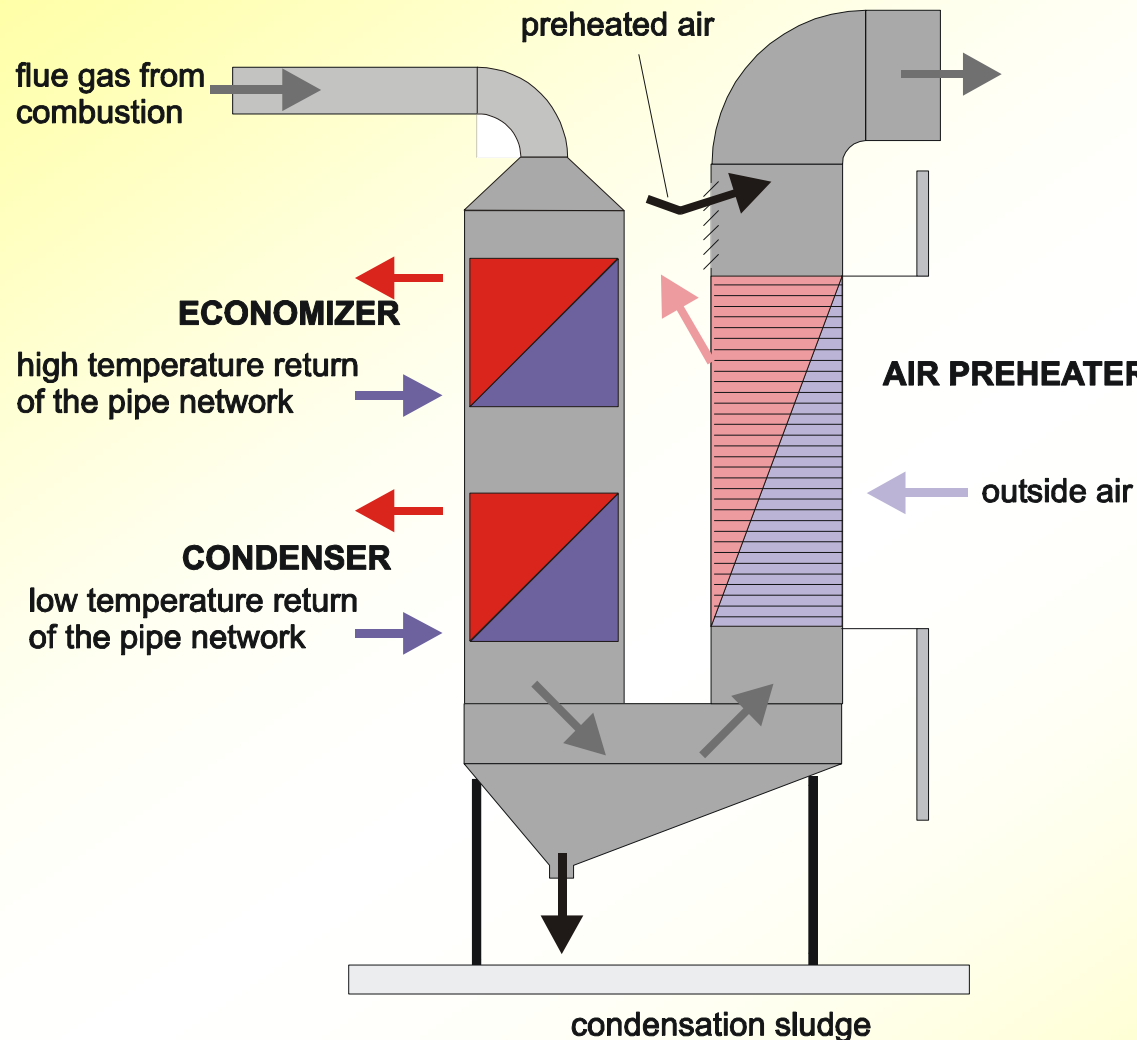
Explanations: all data related to dry flue gas and 13 vol.% O<sub>2</sub>  
ae.d.: aerodynamic particle diameter  
underfeed stoker, full load  
fuel: hardwood (wood chips and sawdust)





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## Flue gas condensation units



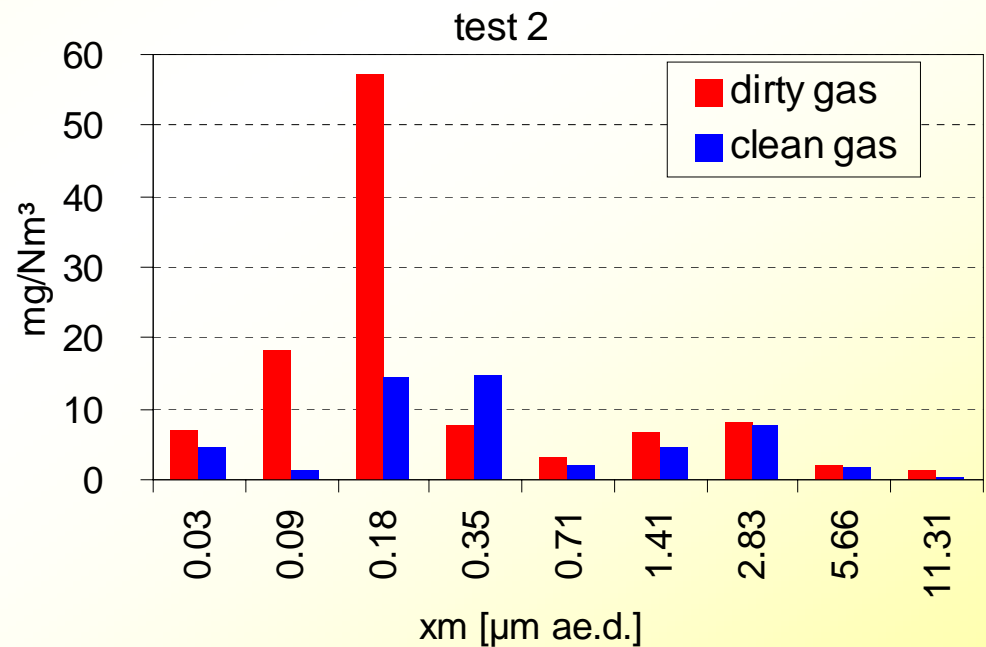
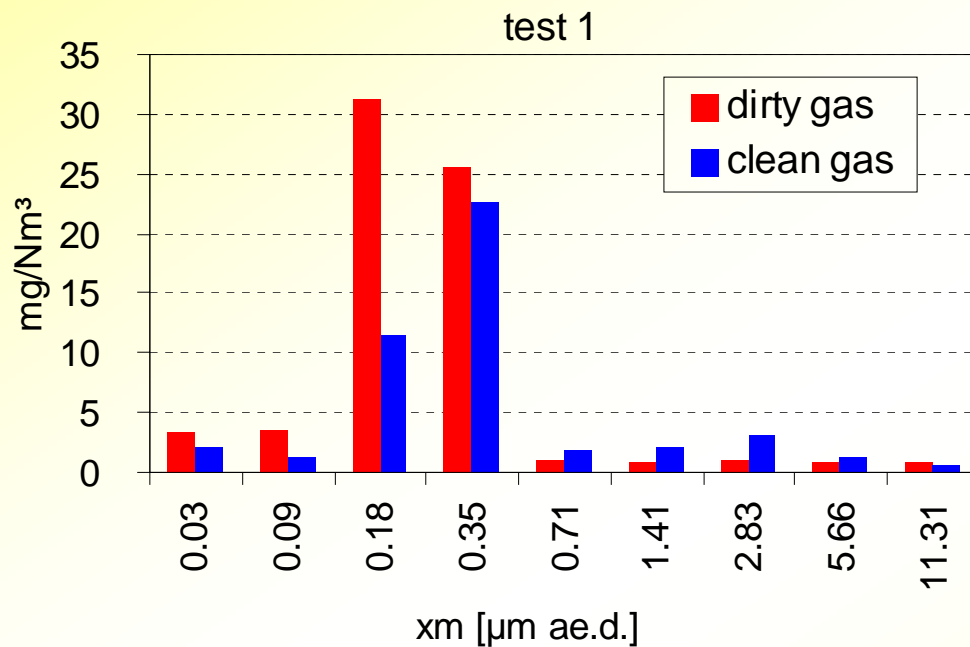
- Combined dust precipitation and recovery of sensible and latent heat
- Not applicable in all biomass combustion units.  
Constraints for application are:
  - low temperature of return
  - high moisture content of fuel
- Particle separation efficiency  
coarse fly ashes: almost 100%  
aerosols: depends on amount of condensed water vapour
- Pre-separation of coarse fly ash particles is recommended to avoid plugging of tube pipes
- Sludge/water separation is necessary
- Heat exchanger tubes can be cleaned by water injection



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## Flue gas condensation units – aerosol precipitation

### Measured particle size distributions of aerosols upstream and downstream a flue gas condensation unit



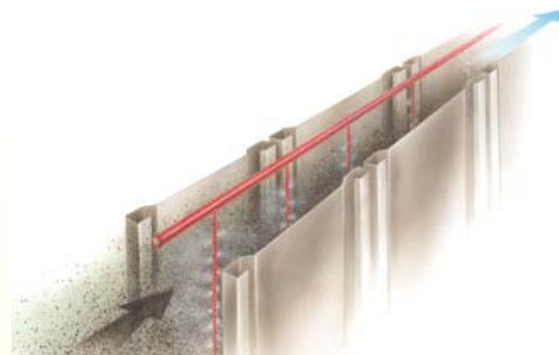
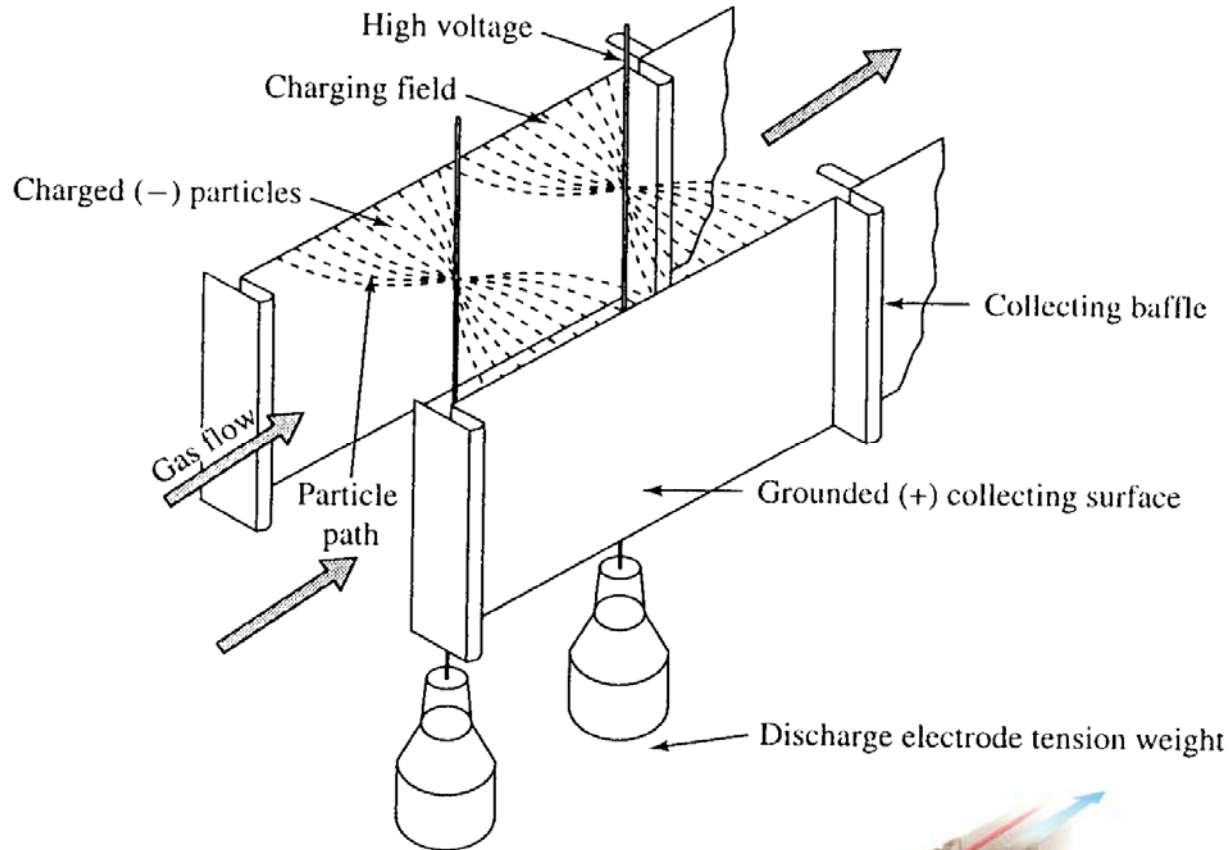
**Aerosol precipitation efficiency: test 1: 39%, test 2: 60%**

Explanations: all data related to dry flue gas and 13 vol.% O<sub>2</sub>; ae.d.: aerodynamic particle diameter; grate-fired combustion unit, 70% load; fuel: bark



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## Electrostatic precipitators - principle of dry ESP



### Principle:

- (1) Particles are charged and
- (2) precipitated at collection electrodes (plates)
- (3) particles are removed from electrodes by rapping

### Required properties of dust:

Specific electric resistivity  
between  $10^7$  and  $10^{11}$  Ohm\*cm

### Operation temperature

up to  $480^{\circ}\text{C}$ , usually  $<250^{\circ}\text{C}$

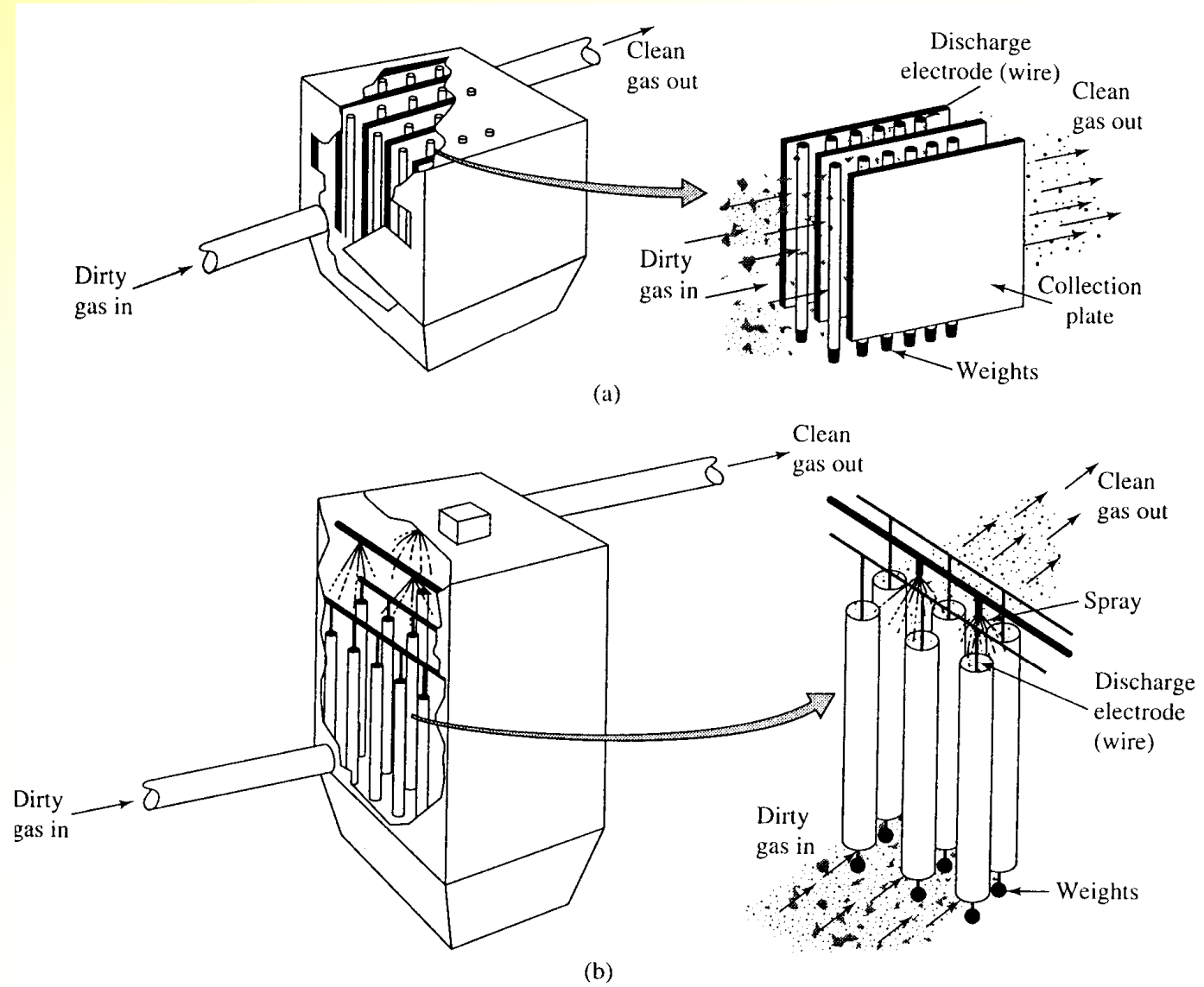
### Operation pressure

up to 20 bar, usually atmospheric



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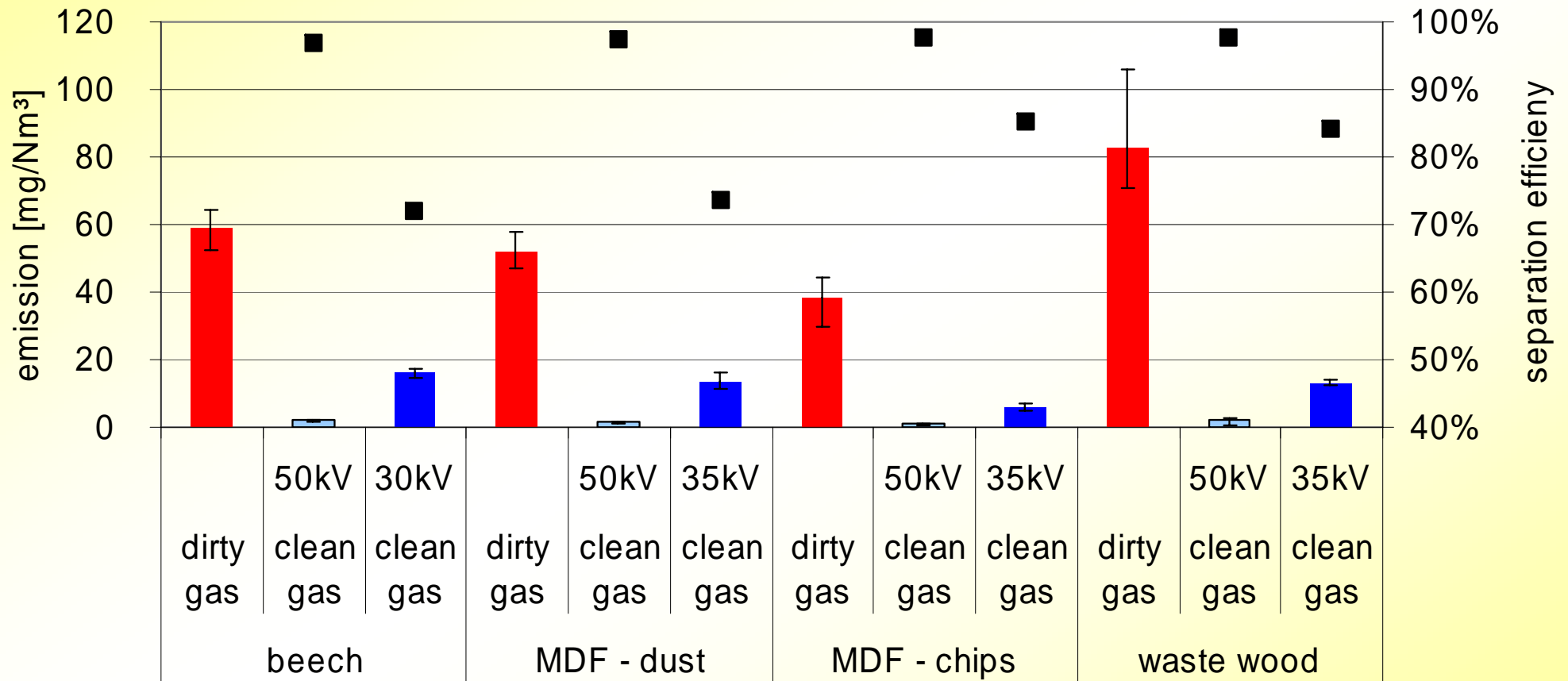
# Electrostatic precipitators - plate and tube-type ESP





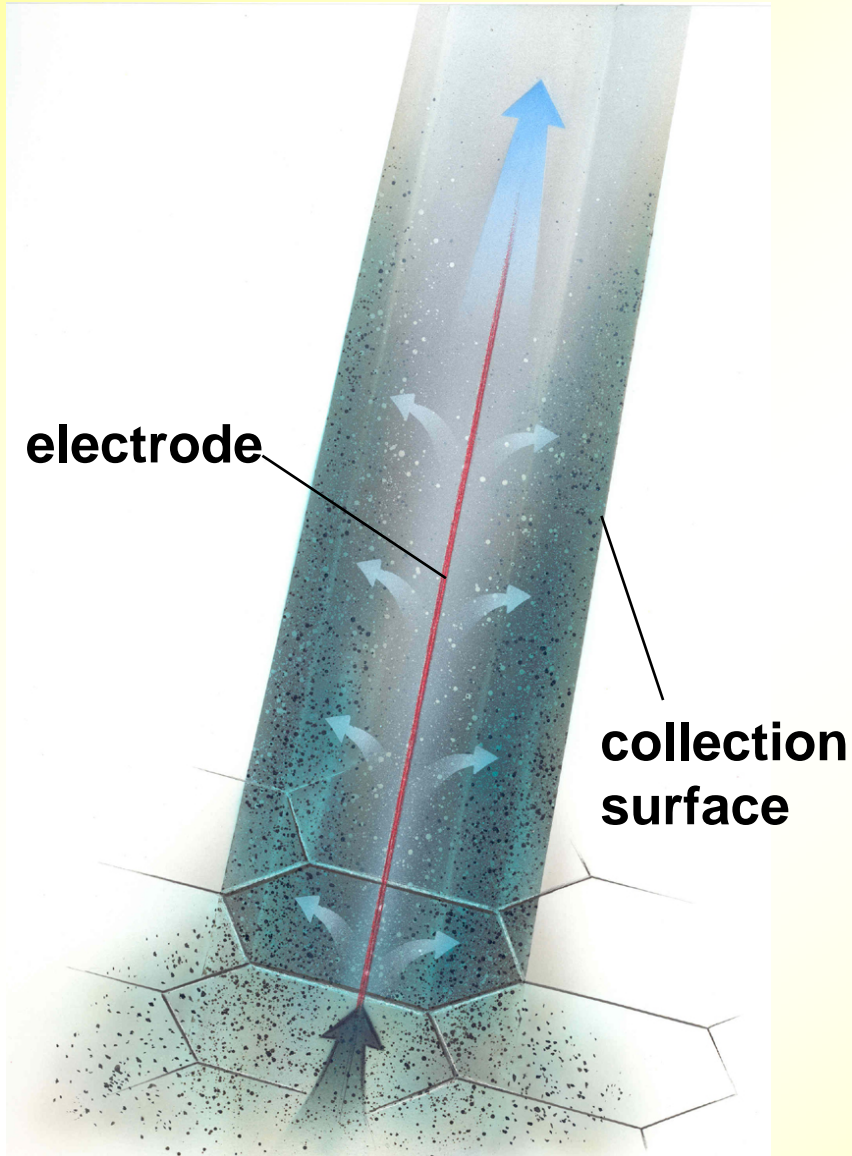
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## Dry electrostatic precipitators – aerosol precipitation vs. voltage



Explanations: results from impactor measurements; only particles <1µm considered  
all data related to dry flue gas and 13 vol.% O<sub>2</sub>  
grate-fired combustion unit; filter current: <2 mA

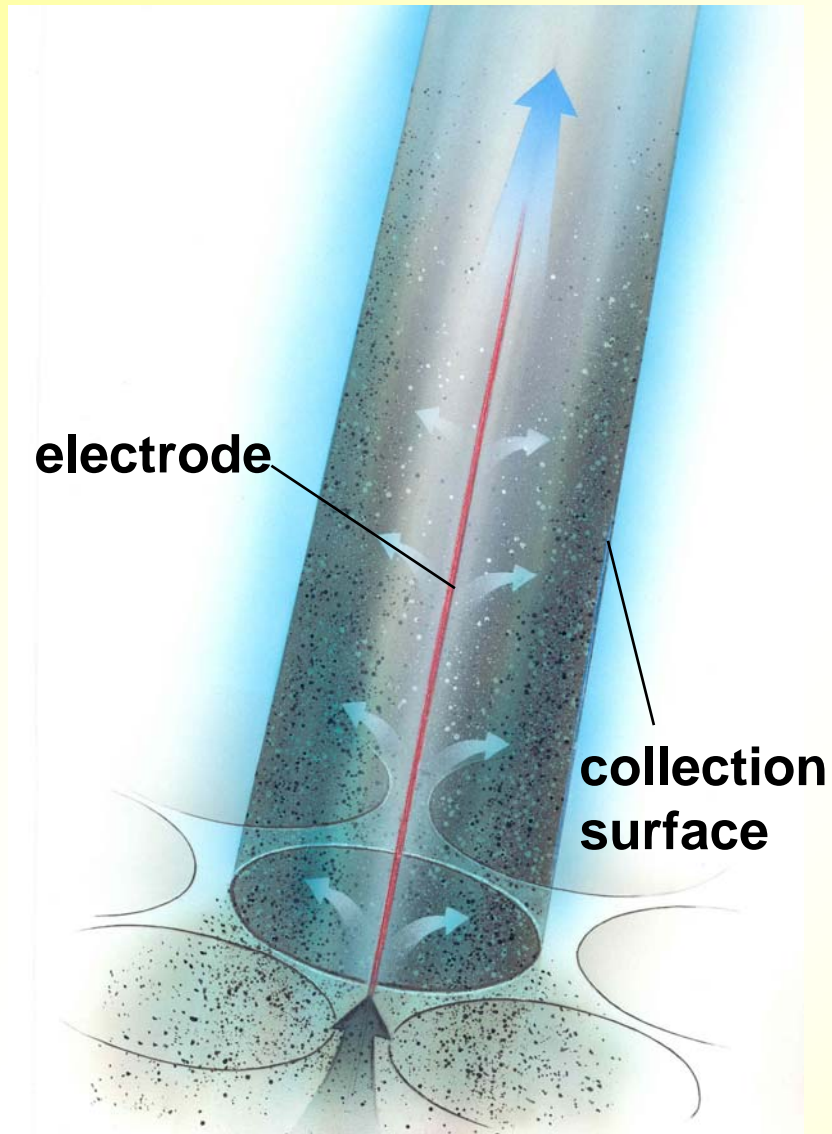
## Electrostatic precipitators - principle of wet ESP (I)



### Principle:

- The flue gas flows vertically through **honeycomb-shaped collection surfaces**.
- An **emission electrode** is located in the centre of the honeycombs.
- Before entering the wet ESP, the flue gas is cooled by a **quenching process** and saturated with water.
- Increasing the amount of moisture in the flue gas reduces the electrical resistance of the dust, making it easier to charge and remove the particles.

## Electrostatic precipitators - principle of wet ESP (II)



### Principle:

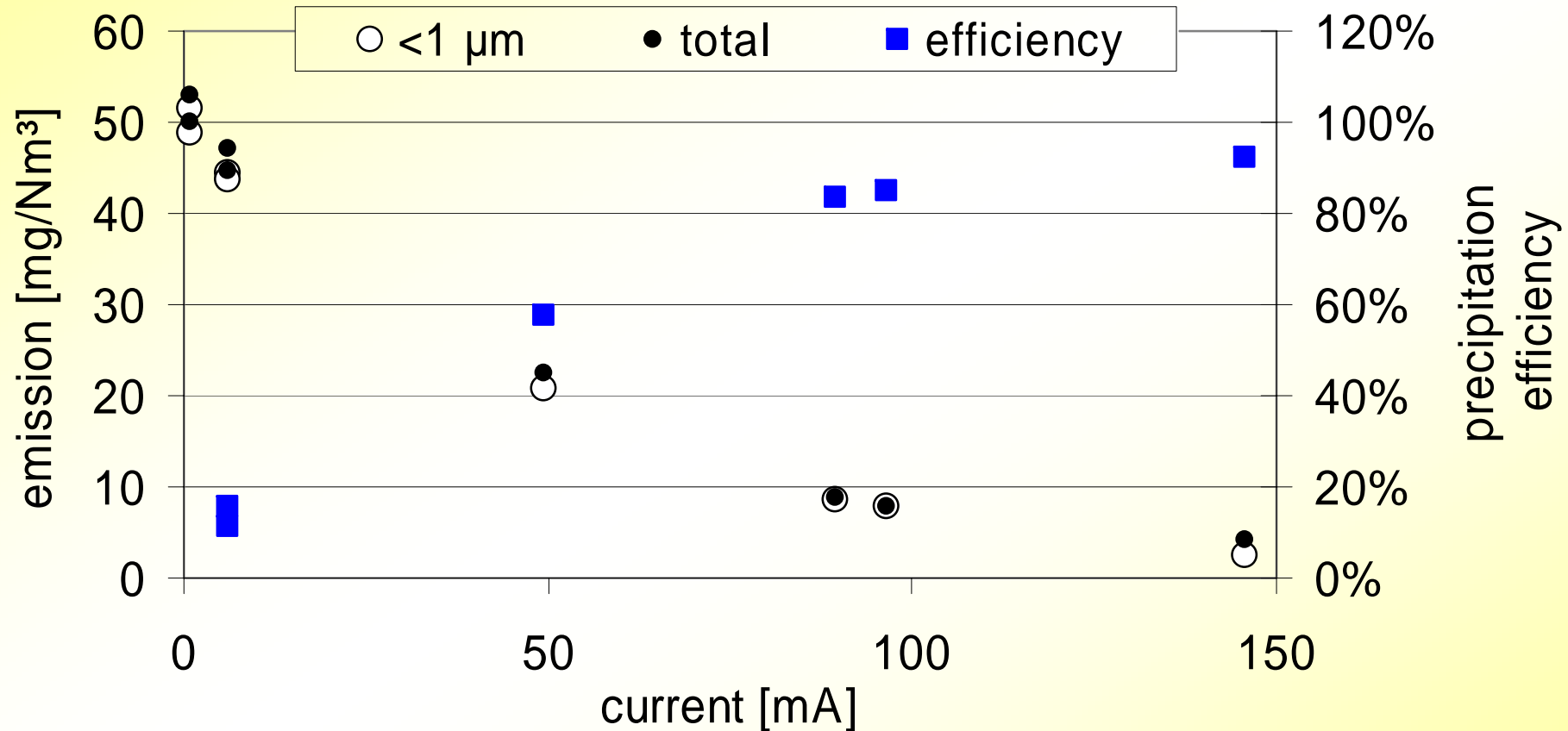
- Collection surfaces are configured as **circular pipes**
- These collection surfaces are **cooled on the outside** by a surrounding flow of ambient air, which causes a layer of condensed vapour on the inside of the pipes
- Disadvantage: **larger overall size**
- Advantage: **enhanced self-cleaning effect** (as the condensate drains off, it creates a film of water that carries away the separated particles)



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## Wet ESP –

## aerosol precipitation vs. filter current



Explanations: results from impactor measurements; <1μm ... particles collected on impactor stages with a cut diameter <1μm; total ... total amount of particles collected with the impactor; all data related to dry flue gas and 13 vol.% O<sub>2</sub>; grate-fired combustion unit; fuel: mixture of bark, wood chips and sawdust; filter voltage: <60 kV





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## Baghouse filters

### Principle:

- Flue gas is filtered on the surface of filter media by cake generation
- The cake is periodically removed from the surface by pressurised air

### Operation temperature

- up to 850°C (depending on filter material)
- usually in the range between 160 and 220°C

### Operation pressure

- up to 50 bar
- usually atmospheric

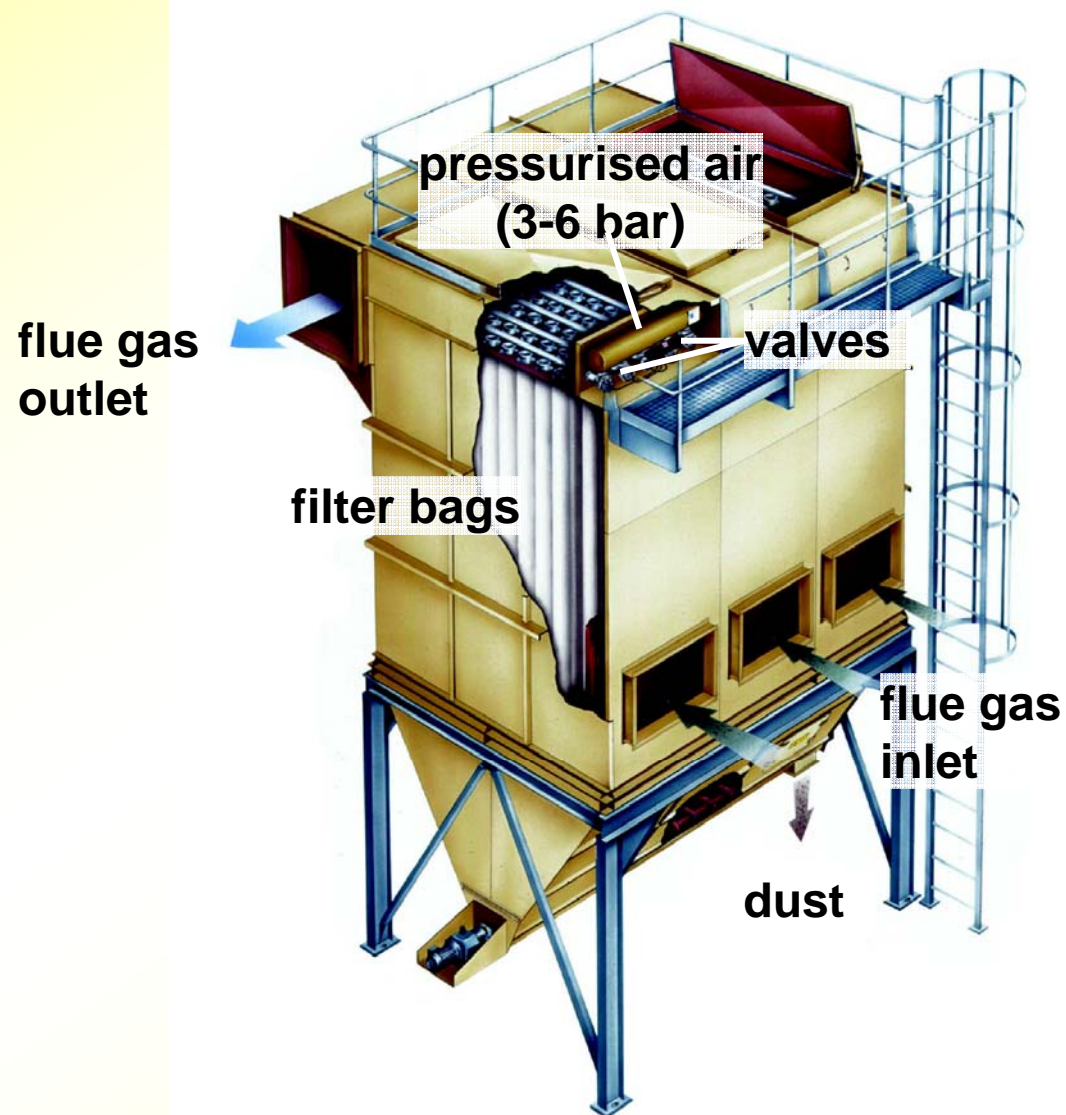
### Additional advantage

- Combination with dry sorption in order to decrease HCl, SO<sub>x</sub>, Hg and PCDD/F emissions



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## Baghouse filters – scheme

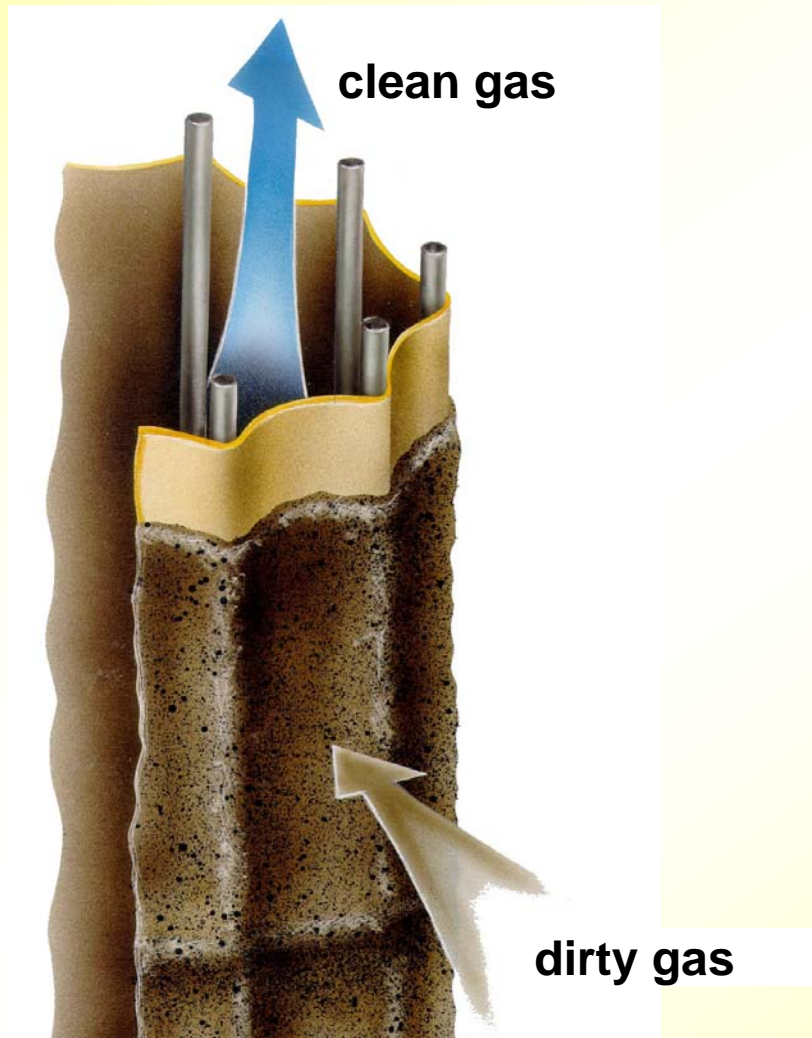




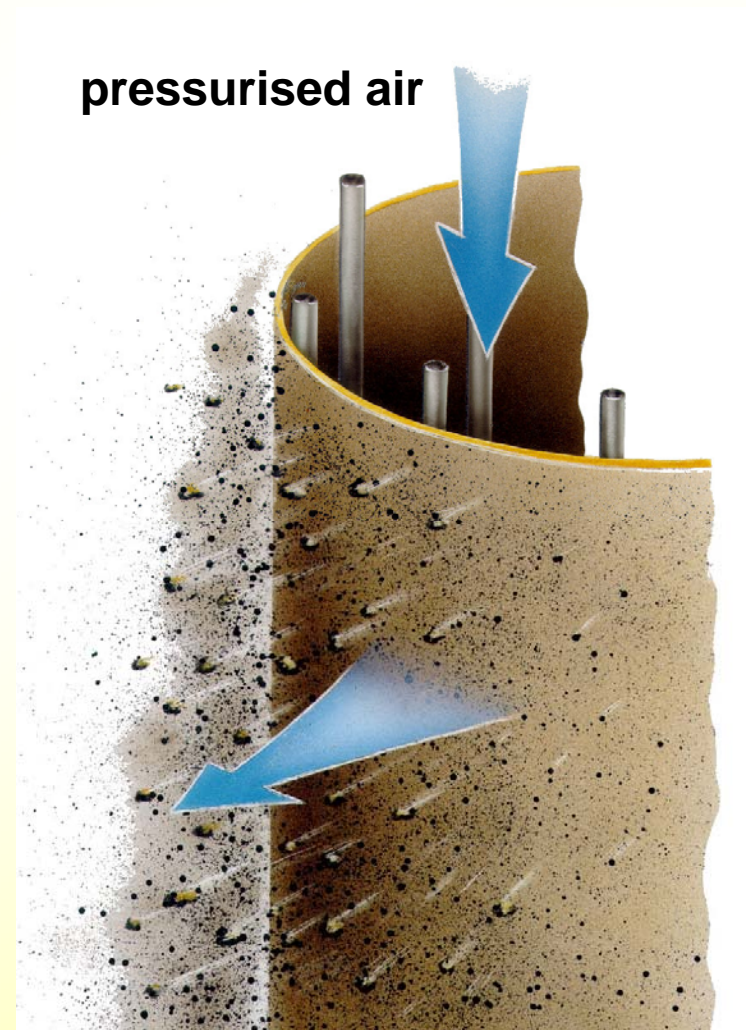
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## Baghouse filters – filter bag cleaning

### filtration



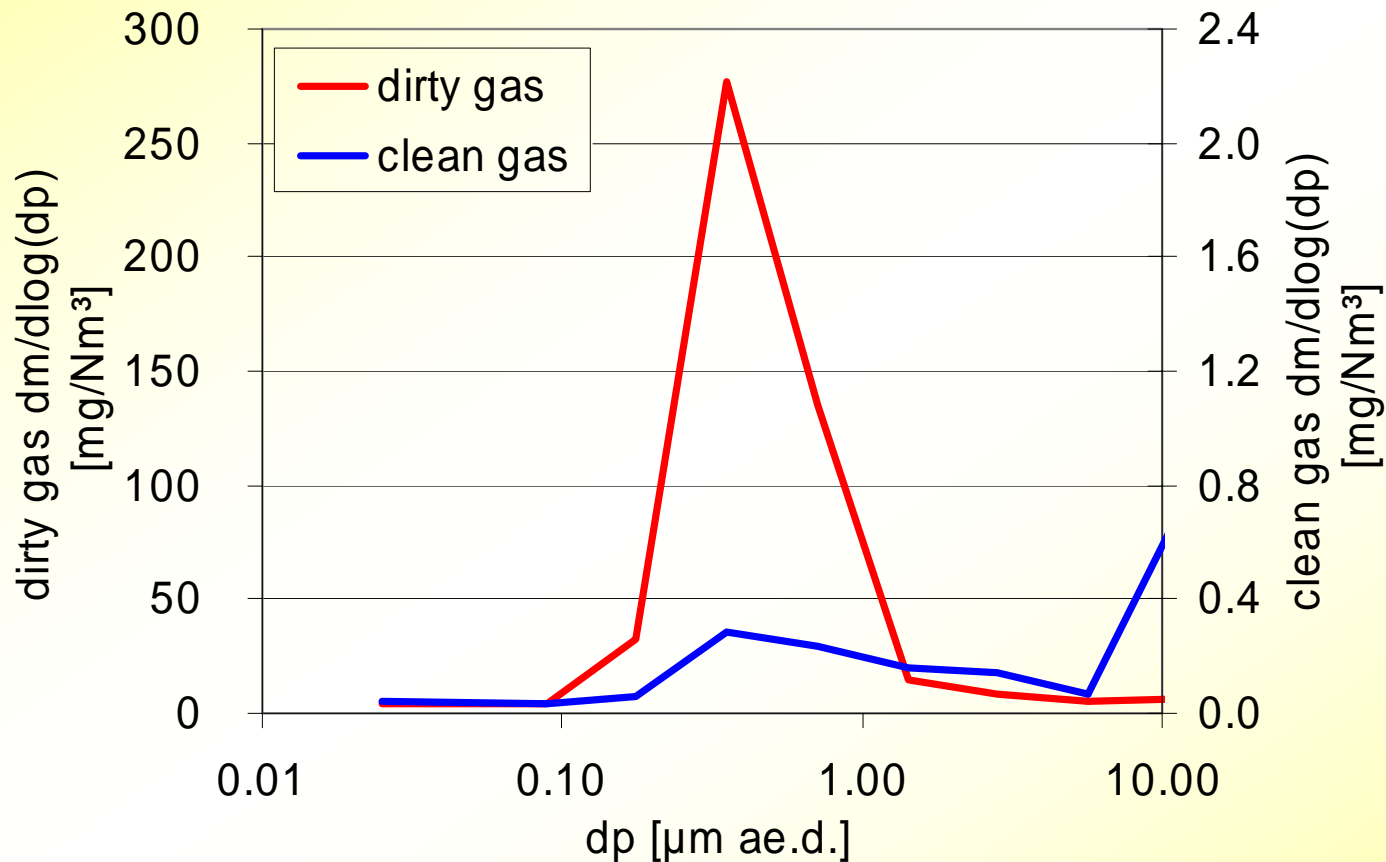
### cleaning





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## Baghouse filters – aerosol precipitation



**Aerosol precipitation efficiency: >99%**

Explanations: results from impactor measurements; all data related to dry flue gas and 13 vol.% O<sub>2</sub>; grate-fired combustion unit; fuel: waste wood

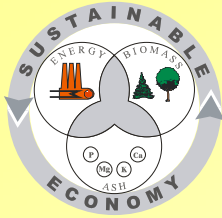


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## Particle separation in biomass combustion units – results from measurements

	multi-cyclone	flue gas cond. unit		ESP 1	ESP 2	baghouse filter
combustion technology	underfeed stoker	moving grate	moving grate	underfeed stoker	moving grate	moving grate
fuel	hardwood	bark	hardwood	hardwood	ind. waste wood	waste wood
load (% nominal capacity)	90	70	50	25	80 - 100	60 - 85
av. total fly ash, dirty gas	109		113	260	132	433
av. total fly ash, clean gas	74		24	<10	32	<2
coarse fly ash precipitation	☒☒☐	☒☒☒	☒☒☒	☒☒☒	☒☒☒	☒☒☒
aerosols, dirty gas	22 – 35	60 – 110	26 – 36	90 – 120	35 – 58	72 – 98
aerosols, clean gas	22 - 35	36 – 55	22 - 26	<10	6 – 8	0.4 – 0.7
aerosol precipitation	☐☐☐	☒☒☐	☒☐☐	☒☒☐	☒☒☐	☒☒☒

Explanation: all data in mg/Nm<sup>3</sup> related to dry flue gas and 13 vol.% O<sub>2</sub>



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## Conclusions and recommendations

**Best applicable precipitation technology with respect to the capacity range and fuel used**

**Emission limit:  $>150 \text{ mg/Nm}^3$**

**multi-cyclone**

**Emission limit:  $50 \text{ mg/Nm}^3$**

**flue gas condensation units,  
dry ESP**

**Emission limit:  $20 \text{ mg/Nm}^3$**

**dry or wet ESP**

**Emission limit:  $10 \text{ mg/Nm}^3$**

**baghouse filters, wet ESP**

**Waste wood fired plants**

**highly efficient baghouse filters**

**Generally, a cyclone or multi-cyclone should be implemented upstream an ESP, baghouse filter or flue gas condensation unit in order to remove the coarse fly ash particles**